

### AMENDMENTS TO THE CLAIMS

1. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing a gasoline blending component, comprising hydrogenating in two steps a mainly olefinic liquid feed-stock comprising olefins; and sulphur compounds as impurities, in the presence of hydrogen and a noble metal catalyst on aluminium oxide support, ~~and~~ wherein in the first step the major part of olefins are converted and in the secondary step the remaining olefins and sulphur compounds react, ~~and~~ wherein a trickle-bed reactor is used in the first step and in the second step, and wherein the feed-stock comprises 80-97 wt % of C<sub>8</sub> olefins, 3-20 wt % of C<sub>12</sub> olefins, and 0.1-7 wt % of C<sub>9</sub>, C<sub>10</sub>, C<sub>11</sub> and heavier >C<sub>12</sub> olefins.

2. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein the hydrogen feed /olefin feed molar ratio is 0.9-2.0.

3. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1 or 2, wherein the feed-stock further comprises ~~80-97 wt % of C<sub>8</sub> olefins, 3-20 wt % of C<sub>12</sub> olefins, 0.1-7 wt % of C<sub>9</sub>, C<sub>10</sub>, C<sub>11</sub> and heavier > C<sub>12</sub> olefins and optionally~~ minor amounts of lighter C<sub>6</sub>-C<sub>7</sub> olefins and 1-1000 wt-ppm of sulphur compounds, calculated as sulphur.

4. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein the feed-stock originates from a mixture obtained from a dimerization of butenes.

5. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein the feed-stock contains as sulphur compounds mainly sulphides, disulphides, thiophene and/or alkylthiophenes.

6. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein the noble metal catalysts comprises < 1 wt% of platinum or/and palladium.

7. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein the noble metal catalysts comprises < 1 wt% of platinum.

8. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein the reaction temperature in the first step is in the range of 150–230°C and the pressure is in the range of 20–70 bar and in the second step the temperature is in the range of 180–300°C and the pressure is in the range of 20–70 bar.

9. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1 wherein the reaction heat is removed from the process and the reaction heat is used for preheating of incoming feed-stock to the a dimerization unit of butenes, or as an energy source for distillation columns of bottom boilers of dimerization unit of butenes.

10. (Cancelled)

11. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein in the first step the product stream is circulated in the reactor(s).

12. (Previously Presented) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein the hydrogen feed /olefin feed molar ratio is 1.0-1.5.